

This listing of claims will replace all prior versions, and listings, of claims in the application:

**Listing of Claims:**

Claim 1 (original): Catalyst comprising at least one zeolite (molecular sieve) chosen from the group formed by the TON structure type zeolites (Theta-1, ZSM-22, ISI-1, NU-10 and KZ-2) and at least one ZBM-30 zeolite synthesized with a particular structuring agent such as triethylenetetramine, at least one hydro-dehydrogenating element, and at least one porous mineral matrix.

Claim 2 (original): Catalyst according to claim 1 in which the hydro-dehydrogenating element is chosen from the elements of Group VIB and Group VIII of the periodic table.

Claim 3 (original): Catalyst according to claim 2 in which the hydro-dehydrogenating element of Group VIB is molybdenum and/or tungsten.

Claim 4 (currently amended): Catalyst according to ~~one of claims 2 to 3~~ claim 2 in which the hydro-dehydrogenating element of Group VIII is a noble metal of Group VIII.

Claim 5 (original): Catalyst according to claim 4 in which the hydro-dehydrogenating element of Group VIII is platinum and/or palladium.

Claim 6 (currently amended): Catalyst according to ~~one of the preceding claims~~ claim 1 subjected to sulphurization treatment.

Claim 7 (original): Process for improving the pour point of a paraffin charge, in which the charge to be treated is brought into contact with a dewaxing catalyst comprising at least one zeolite (molecular sieve) chosen from the group formed by the TON structure type zeolites (Theta-1, ZSM-22, ISI-1, NU-10 and KZ-2) and at least one ZBM-30 zeolite synthesized with a

particular structuring agent such as triethylenetetramine, at least one hydro-dehydrogenating element and at least one porous matrix.

Claim 8 (original): Process according to claim 7 in which the treated charges contain at least 20% by volume of compounds boiling above 340°C.

Claim 9 (currently amended): Process according to ~~one of claims 7 to 8~~ claim 7 in which the operating conditions are the following:

- the reaction temperature is between 200 and 450°C,
- the pressure is between 0.1 and 25 MPa,
- the hourly volume rate (hvr expressed as volume of charge injected per volume unit of catalyst per hour) is between approximately 0.05 and approximately 30h<sup>-1</sup>.

Claim 10 (currently amended): Process according to ~~one of claims 7 to 9~~ claim 7 in which the charge undergoes a hydroisomerization-hydroconversion stage beforehand.

Claim 11 (original): Process according to claim 10 in which all of the effluent from the hydroisomerization-conversion stage is sent to the dewaxing catalyst.

Claim 12 (currently amended): Process according to ~~one of claims 10 to 11~~ claim 10 in which the hydroisomerization-hydroconversion stage is preceded by a hydrorefining stage.

Claim 13 (original): Process according to claim 12 in which the hydrorefining stage is followed by an intermediate separation.

Claim 14 (currently amended): Process according to ~~one of claims 7 to 13~~ claim 7 in which the effluent from the catalytic hydrodewaxing stage is at least partly sent to a hydrofinishing catalyst.